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# Nonlinear evolution of vortical disturbances entrained in the entrance region of a circular pipe

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The nonlinear evolution of free-stream vortical disturbances entrained in the entrance 7 region of a circular pipe is investigated using asymptotic and numerical methods. Attention 8 is focused on the low-frequency disturbances that induce streamwise elongated structures. A 9 pair of vortical modes with opposite azimuthal wavenumbers is used to model the free-stream 10 disturbances. Their amplitude is assumed to be intense enough for nonlinear interactions to 11 occur inside the pipe. The formation and evolution of the perturbation flow are described 12 by the nonlinear unsteady boundary-region equations in the cylindrical coordinate system, 13 derived and solved herein for the first time. Matched asymptotic expansions are employed 14 to construct appropriate initial conditions and the initial-boundary value problem is solved 15 numerically by a marching procedure in the streamwise direction. Numerical results show 16 the stabilising effect of nonlinearity on the intense algebraic growth of the disturbances and 17 an increase of the wall-shear stress due to the nonlinear interactions. A parametric study 18 19 is carried out to evince the effect of the Reynolds number, the streamwise and azimuthal wavelengths, and the radial length scale of the inlet disturbance on the nonlinear flow 20 evolution. Elongated pipe-entrance nonlinear structures (EPENS) occupying the whole pipe 21 cross-section are discovered. EPENS with h-fold rotational symmetry comprise h high-22 speed streaks positioned near the wall, and h low-speed streaks centred around the pipe core. 23 These distinct structures display a striking resemblance to nonlinear travelling waves found 24 numerically and observed experimentally in fully developed pipe flow. Good agreement of 25 our mean-flow and root mean square data with experimental measurements is obtained. 26

## 27 Key words:

## 28 1. Introduction

As one of the most long-standing problems in fluid dynamics, stability and transition in pipe flow have puzzled engineers and scientists since the prominent experimental work of Reynolds (1883). Due to wide industrial applications, engineers have aimed to design efficient and durable pipeline systems by estimating the conditions under which the pipe flow

- 33 is laminar or turbulent. This objective is driven by the large difference in pressure gradient
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<sup>34</sup> required to drive laminar and turbulent flows in a pipe. Scientists have also been intrigued by

the enigmatic physical mechanisms behind the instability and transition phenomena observed in experiments.

Earlier investigations of pipe flow date back to the independent studies of Hagen (1839) 37 and Poiseuille (1844), where the linear relationship between pressure drop and volume flow 38 rate for laminar flow was obtained. This relationship is now known as the Hagen-Poiseuille 39 40 law, which holds only sufficiently downstream where the flow is fully developed, i.e. the velocity distribution is independent of the streamwise coordinate and its profile is parabolic. 41 Near the pipe inlet, the velocity field varies in the streamwise direction and the terminologies 42 developing pipe flow and pipe entrance flow are adopted. Considerable research effort has 43 been focused on the stability and transition of the fully developed region, but much less 44 attention has been devoted to the flow in the entrance region of the pipe. In this paper, we 45 thus aim to investigate how free-stream vortical disturbances are entrained in the entrance 46 region of a circular pipe and how the induced disturbances grow and evolve nonlinearly 47 inside the pipe. 48

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## 1.1. Fully developed pipe flow

The stability and transition of fully developed laminar pipe flow cannot be explained by the 50 classical linear stability theory because the parabolic profile is stable to infinitesimally small 51 disturbances. The reader is referred to Rayleigh (1892), Sexl (1927), Pekeris (1948), Corcos 52 & Sellars (1959) and Gill (1965) for theoretical studies, and to Davey & Drazin (1969), 53 Crowder & Dalton (1971), Garg & Rouleau (1972), Salwen & Grosch (1972) and Meseguer 54 & Trefethen (2003) for numerical studies. However, transition in pipe flow is usually observed 55 in experiments at moderate Reynolds numbers. This discrepancy has led to the inclusion of 56 nonlinear effects in the study of pipe-flow stability. Weakly nonlinear theory was first applied 57 independently by Davey & Nguyen (1971) and Itoh (1977), but the results contradicted 58 each other. Davey & Nguyen (1971) reported that fully developed pipe flow was unstable 59 to small but finite axisymmetric centre-mode disturbances when the disturbance amplitude 60 exceeded a critical value, while the flow was found to be stable by Itoh (1977). The problem 61 was reexamined by Davey (1978), who suggested that neither of those results was reliable. 62 Direct numerical simulations performed by Patera & Orszag (1981) failed to find any finite-63 amplitude axisymmetric equilibria and suggested that the use of weakly nonlinear theory 64 65 away from the neutral stability curve may be invalid. Smith & Bodonyi (1982) identified neutral disturbances of finite amplitude by employing the nonlinear critical layer theory. 66

The research interest then shifted from solving the eigenvalue problem established by 67 the modal stability theory to the temporal initial value problem pertaining to the non-68 modal stability theory. Since the linear stability theory captures the long-time disturbance 69 behaviour but overlooks the short-time behaviour (Kerswell 2005; Schmid 2007), at short 70 times, disturbances may experience algebraic transient growth before the ultimate exponential 71 decay (e.g., Böberg & Brösa 1988). One related approach is to identify the optimal disturbance 72 that achieves the maximum transient energy growth. Studies on transient growth in time 73 have revealed that optimal disturbances have a vanishing streamwise wavenumber and a 74 unity azimuthal wavenumber (Bergström 1992; Schmid & Henningson 1994; O'Sullivan & 75 Breuer 1994). Bergström (1993) and Schmid & Henningson (1994) also extended the work to 76 disturbances with small but non-zero streamwise wavenumber. The spatial transient growth 77 has been reported by Tumin (1996) and Reshotko & Tumin (2001). Stationary disturbances 78 were found to exhibit a more significant amplification than non-stationary ones (Reshotko 79 & Tumin 2001). Optimal disturbances provide the upper bound for the possible energy 80 81 amplification, which is optimised over all possible initial conditions.

82 Faisst & Eckhardt (2003) and Wedin & Kerswell (2004) independently discovered

nonlinear travelling waves in pipe flow for the first time, which were later observed in 83 the experiments of Hof et al. (2004) and Hof et al. (2005). Inspired by these results, the 84 nonlinear dynamical system approach has become a valuable tool in the last two decades 85 (Eckhardt et al. 2007; Avila et al. 2023). From the perspective of dynamical theory, all initial 86 conditions of the pipe-flow system that ultimately converge to the laminar state form the basin 87 of attraction of the laminar state. Transition occurs when the initial conditions are outside 88 89 of this basin boundary. The nonlinear non-modal stability theory describes the dynamics of finite disturbances within and beyond the basin boundary (Kerswell et al. 2014; Kerswell 90 2018). Optimisation methods have been utilised within this nonlinear theory to compute the 91 so-called minimal seed (Pringle & Kerswell 2010; Pringle et al. 2012), i.e. the disturbance 92 with the smallest energy for turbulence to occur. The interested reader is referred to Kerswell 93 (2018) for an exhaustive review. 94

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## 1.2. Pipe-entrance flow

The absence of linear instability in fully developed pipe flow directed interest to the flow in the developing entrance region. As the uniform flow enters the pipe inlet, a laminar boundary layer grows along the wall. One can then expect this pipe-entrance boundary layer to be linearly unstable. Research efforts first focused on the computation of the velocity and pressure distributions of this base flow (Langhaar 1942; Hornbeck 1964; Sparrow *et al.* 1964; Christiansen & Lemmon 1965).

The first temporal stability analysis of the pipe entrance flow was performed by Tatsumi 102 (1952) by using a boundary-layer model that revealed the linear instability of the flow 103 subjected to axisymmetric disturbances. The same problem was investigated numerically by 104 Huang & Chen (1974a) and generalised to non-axisymmetric disturbances (Huang & Chen 105 1974b; Shen et al. 1976) and spatially unstable disturbances (Gupta & Garg 1981; Garg 106 1981; Garg & Gupta 1981; Garg 1983). Considerable discrepancies were observed among 107 the results obtained in these studies, which may be attributed to the varying accuracies in 108 the calculation of the laminar base flow (da Silva & Moss 1994). da Silva & Moss (1994) 109 reexamined this stability problem with improved accuracy, obtaining good agreement with 110 results by Gupta & Garg (1981). The critical Reynolds number based on the pipe radius was 111 approximately 10 000 in both studies. 112

Although these studies focused on the stability of flow profiles at different streamwise 113 locations in the pipe entrance, the receptivity problem - i.e. how entrained free-stream 114 disturbances excite instability in the entrance region - was not considered. This problem is, 115 however, of central importance because, as even remarked by Reynolds (1883), the pipe inlet 116 disturbances have a significant effect on the stability and laminar-turbulent transition of the 117 pipe-entrance flow. By controlling the disturbance level at the pipe inlet, the flow studied by 118 Reynolds (1883) was maintained laminar up to Reynolds numbers ranging from 2000 to 13 119 000. This number was further increased to 100 000 in the experiments of Pfenniger (1961). 120 Given the importance of the inlet perturbations, it is thus surprising that only a limited 121 number of studies exist on this problem. In the experiments of Sarpkaya (1975), disturbances 122 were introduced on the surface of the pipe entrance, and the occurrence of instability was 123 confirmed. The reported critical Reynolds number was much lower than that estimated by 124 125 theoretical studies, which may be ascribed to the finite-amplitude disturbances induced in the entrance flow. The dynamics of localised turbulence, i.e. puffs and slugs, was studied 126 in the experimental work of Wygnanski & Champagne (1973), where the disturbances were 127 introduced at the pipe inlet using a honeycomb, an orifice plate and a circular disk. Wygnanski 128 et al. (1975) further investigated the propagation of turbulent puffs initiated by an impulsive 129 disturbance at the entrance region. The experimental study of Zanoun et al. (2009) focused 130

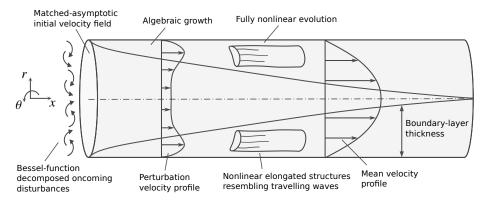


Figure 1: Schematic of the entrance region of a pipe (not to scale).

on the effect of the inlet flow conditions on the flow transition in pipe and channel flows.Different transition Reynolds numbers were measured at different streamwise positions.

Direct numerical simulations were conducted by Wu *et al.* (2015) and Wu *et al.* (2020) to investigate the flow transition to fully developed turbulence triggered by localised inlet disturbances. In Wu *et al.* (2015), the fully developed parabolic laminar velocity profile was chosen as the inlet base flow in most cases, and the plug flow was utilised in one case. The most intense inlet disturbances required to trigger transition pertained to the latter case.

Under the small-amplitude assumption, Ricco & Alvarenga (2022) performed the first 138 theoretical study of the entrainment of free-stream vortical disturbances in the pipe entrance. 139 Their interest was in how these disturbances are affected by the pipe confinement, and on 140 how they grow and develop downstream. The perturbation flow at the pipe inlet was obtained 141 by a matched asymptotic composite solution between a Bessel function vortical flow in the 142 pipe core and a boundary-layer flow near the pipe wall. A streamwise-elongated streaky flow 143 formed within the base-flow boundary layer and evolved towards the pipe centreline farther 144 downstream. A good agreement between the computed velocity profiles and the available 145 experimental data was found when the measured free-stream disturbances were weak. 146

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## 1.3. Objectives

We investigate the entrainment of flow disturbances into the entrance of a circular pipe, and 148 the downstream growth and evolution of the induced nonlinear vortical disturbances along the 149 entrance region. The oncoming disturbances are physically realistic, i.e. they can be generated 150 at the pipe inlet in a laboratory. The nonlinear boundary-region equations are derived in the 151 cylindrical geometry for the first time, and solved numerically by marching downstream. Our 152 study is the nonlinear extension of Ricco & Alvarenga (2022), and the first theoretical study 153 of the entrainment and downstream evolution of finite-amplitude disturbances in the entrance 154 region of a circular pipe. 155

In §2, the scaling and assumptions are presented, together with the mathematical formulation and numerical procedures. Numerical results are discussed in §3. A summary and conclusions are given in §4.

## 159 2. Mathematical formulation and numerical procedures

We consider a circular pipe of radius  $R^*$  described by a cylindrical coordinate system  $\{x^*, r^*, \theta\}$ , where  $x^*$  and  $r^*$  are the streamwise and radial directions, and  $\theta$  is the azimuthal angle. The pipe inlet is located at  $x^* = 0$ , while the pipe axis and the pipe wall are at  $r^* = 0$ 

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and  $r^* = R^*$ , respectively. The superscript \* refers to dimensional quantities hereafter. A schematic of the flow is shown in figure 1.

A pressure-driven incompressible flow is assumed to enter the pipe with a uniform velocity 165  $U_{\infty}^{*}$  at  $x^{*} = 0$ . Superimposed on the oncoming flow are small-amplitude gust-type vortical 166 fluctuations that can be modelled by a Fourier–Bessel series with Fourier expansions in  $x^*$ ,  $\theta$ 167 and time  $t^*$ , and a Bessel expansion in  $r^*$ . A pair of vortical modes with the same frequency  $f^*$ 168 (and hence the same streamwise wavenumber  $k_x^*$ ), but opposite azimuthal wavenumbers  $\pm m_0$ , 169 is considered ( $m_0 \ge 0$  is taken without losing generality). The circumferential wavelength 170 of the free-stream gust at the pipe radius,  $\lambda^* = 2\pi R^*/m_0$ , is chosen as the reference length. 171 The velocities and time are normalised by  $U_{\infty}^*$  and  $\lambda^*/U_{\infty}^*$ , respectively, while the pressure 172  $p^*$  is normalised by  $\rho^* U_{\infty}^{*2}$ , where  $\rho^*$  is the density of the fluid. 173

Following Ricco & Alvarenga (2022), a single pair of free-stream gusts is passively advected by  $U_{\infty}^*$  and expressed as

$$\boldsymbol{u} - \{1, 0, 0\} = \epsilon \left\{ \hat{\boldsymbol{u}}_{+, \boldsymbol{m}_{0}}^{\infty} e^{i m_{0} \theta} + \hat{\boldsymbol{u}}_{-, \boldsymbol{m}_{0}}^{\infty} e^{-i m_{0} \theta} \right\} e^{i k_{x}(x-t)} + \text{c.c.},$$
(2.1)

177 where

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178 
$$\hat{\boldsymbol{u}}_{\pm,\boldsymbol{m}_{0}}^{\infty}(r;l) = \left\{ \hat{u}_{m_{0}}^{\infty}J_{m_{0}}(r_{0}), \frac{\hat{v}_{m_{0}}^{\infty}J_{m_{0}}(r_{0})}{r_{0}}, \frac{\mp i\hat{w}_{m_{0}}^{\infty}J_{m_{0}}'(r_{0})}{\xi_{m_{0},l}} \right\} = O(1).$$
(2.2)

179 Here,  $\boldsymbol{u} = \{u, v, w\}$  corresponds to the velocity components in the x, r and  $\theta$  directions,  $\epsilon \ll 1$ is a measure of the amplitude of the disturbances, the quantities  $\{\hat{u}_{m_0}^{\infty}, \hat{v}_{m_0}^{\infty}, \hat{w}_{m_0}^{\infty}\} = O(1)$  are 180 complex,  $J_{m_0}$  is the Bessel function of the first kind of order  $m_0$ ,  $r_0 = r\xi_{m_0,l}/2R$  with  $\xi_{m_0,l}$ 181 being the *l*th zero of the Bessel function  $J_{m_0}$ , and c.c. denotes the complex conjugate. The 182 notations  $m_0$  and  $r_0$  correspond to m and  $\overline{r}$  in Ricco & Alvarenga (2022). A similar expansion 183 184 of the free-stream vortical disturbances has been used in Ricco et al. (2011) and Marensi et al. (2017) for flat-plate boundary layers, Marensi & Ricco (2017) for concave boundary 185 layers, and Ricco & Alvarenga (2021) for a channel flow. The expansion (2.1)–(2.2) is a 186 model of free-stream vortical disturbances that could be realised in a laboratory by a grid of 187 vibrating ribbons, a polar equivalent of the careful receptivity studies of Dietz (1999) and 188 189 Borodulin et al. (2021).

Our focus is on oncoming disturbances with a long streamwise wavelength (i.e. low frequency), i.e.  $k_x \ll 1$ , which have been experimentally demonstrated to be the most likely to penetrate into a boundary layer and form streamwise-elongated structures (Matsubara & Alfredsson 2001). Under the low-frequency assumption, the continuity equation of the gust disturbances becomes

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$$\xi_{m_0,l}\hat{v}_{m_0}^{\infty} + m_0\hat{w}_{m_0}^{\infty} = 0, \qquad (2.3)$$

196 where  $\partial u / \partial x = O(k_x) \ll 1$  has been neglected.

As the oncoming flow enters the pipe, a boundary layer develops on the pipe wall. As 197 the flow evolves downstream, the boundary-layer thickness becomes comparable with the 198 azimuthal wavelength  $\lambda^*$  at  $x = O(Re_{\lambda})$ , where  $Re_{\lambda} = U_{\infty}^* \lambda^* / v^* \gg 1$ , and  $v^*$  is the kinematic 199 viscosity of the fluid. A distinguished scaling is  $k_x = O(Re_{\lambda}^{-1})$ , and the two slow variables 200 scaled by  $k_x$  are  $\bar{t} = k_x t = O(1)$  and  $\bar{x} = k_x x = O(1)$ . In this region, viscous-diffusion 201 effects in the radial and azimuthal directions are comparable. The flow can be described by 202 the nonlinear boundary-region equations (Ricco et al. 2011), written and solved herein in 203 cylindrical coordinates for the first time. The linear counterpart of these equations, obtained 204 for the turbulent Reynolds number  $r_t = \epsilon R e_\lambda \ll 1$ , was derived and solved in Ricco & 205 Alvarenga (2022) for studying the growth of small-amplitude disturbances. The current 206 207 research relaxes the linear assumption because  $r_t = O(1)$ . Nonlinear interactions are thus taken into account. 208

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## 2.1. Governing equations

210 The boundary-region equations are derived from the incompressible Navier-Stokes equations

$$\nabla \cdot \boldsymbol{u} = 0, \tag{2.4}$$

209

$$\frac{\partial \boldsymbol{u}}{\partial t} + (\boldsymbol{u} \cdot \nabla)\boldsymbol{u} = -\nabla p + \frac{1}{Re_{\lambda}}\nabla^{2}\boldsymbol{u}.$$
(2.5)

The velocity u and the pressure p are decomposed into the laminar base flow and the perturbation flow, namely

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$$\{\boldsymbol{u}, p\} = \{\boldsymbol{U}, P\} + \{\tilde{\boldsymbol{u}}, \tilde{p}\}$$
  
=  $\{U(\bar{x}, r), k_x V(\bar{x}, r), 0, P(\bar{x})\} + r_t \left\{\bar{u}, k_x \bar{v}, k_x \bar{w}, \frac{k_x}{Re_\lambda} \bar{p} + \Gamma(\bar{x})\right\},$  (2.6)

where the perturbation flow is expressed as a Fourier series in  $\theta$  and *t*:

218 
$$\{\bar{u}, \bar{v}, \bar{w}, \bar{p}, \Gamma\} = \sum_{m,n=-\infty}^{\infty} \{\hat{u}_{m,n}, \hat{v}_{m,n}, \hat{w}_{m,n}, \hat{p}_{m,n}, \hat{\Gamma}_{m,n}\} e^{im\theta + in\bar{t}}.$$
 (2.7)

The pressure correction  $\Gamma(\bar{x})$  ensures that the mass flow rate is conserved at each streamwise location and time instant as the modes  $\hat{u}_{0,n}$  are generated by the nonlinear interactions. Therefore,  $\hat{\Gamma}_{m,n} \neq 0$  only if m = 0. As the physical quantities are real, the Hermitian property applies, i.e.

(
$$\hat{q}_{m,n}$$
)<sub>c.c.</sub> =  $\hat{q}_{-m,-n}$ , (2.8)

where  $\hat{q}_{m,n}$  represents any Fourier coefficient  $\{\hat{u}_{m,n}, \hat{v}_{m,n}, \hat{w}_{m,n}, \hat{p}_{m,n}, \hat{\Gamma}_{m,n}\}$  in (2.7).

Substituting (2.6) and (2.7) into the full Navier-Stokes equations (2.4)–(2.5), and taking the limits  $k_x^{-1}$ ,  $Re_\lambda \to \infty$  with  $\mathcal{F} = k_x Re_\lambda = O(1)$  leads to the boundary-layer equations governing the laminar base flow  $\{U, V, P\}$  and to the unsteady nonlinear boundary-region equations governing the perturbation flow  $\{\hat{u}_{m,n}, \hat{v}_{m,n}, \hat{p}_{m,n}, \hat{\Gamma}_{m,n}\}$ .

229 The laminar boundary-layer equations read (Hornbeck 1964)

230 
$$\frac{\partial U}{\partial \bar{x}} + \frac{V}{r} + \frac{\partial V}{\partial r} = 0, \qquad (2.9)$$

231 
$$U\frac{\partial U}{\partial \bar{x}} + V\frac{\partial U}{\partial r} = -\frac{\mathrm{d}P}{\mathrm{d}\bar{x}} + \frac{1}{\mathcal{F}}\left(\frac{1}{r}\frac{\partial U}{\partial r} + \frac{\partial^2 U}{\partial r^2}\right). \tag{2.10}$$

Equation (2.9) and (2.10) are solved together with the conservation of mass flow rate at each streamwise location,

234 
$$\int_{0}^{R} Ur dr = \frac{R^2}{2},$$
 (2.11)

and are subject to the no-slip and no-penetration conditions at the wall and the symmetry conditions at the pipe axis:

237 
$$r = R: \quad U = V = 0,$$
 (2.12)

238 
$$r = 0$$
:  $\frac{\partial U}{\partial r} = 0, V = 0.$  (2.13)

239 The initial condition is obtained by a matched asymptotic combination of the Blasius flow

241 near the pipe wall and an inviscid flow around the pipe core (Ricco & Alvarenga 2022),

$$U(x,r) = \frac{\mathrm{d}F}{\mathrm{d}\eta} - \frac{\beta i^{1/2}}{2\sqrt{2\pi}Re_{\lambda}^{1/2}} \int_{-\infty+i\gamma}^{+\infty+i\gamma} \frac{e^{i\zeta x}}{\zeta^{1/2}I_{1}(\zeta R)} \left[ \frac{I_{1}(\zeta r)}{\zeta r} + I_{1}'(\zeta r) \right] \mathrm{d}\zeta + \frac{\beta i^{1/2}}{2\sqrt{2\pi}Re_{\lambda}^{1/2}} \int_{-\infty+i\gamma}^{+\infty+i\gamma} \frac{e^{i\zeta x}}{\zeta^{1/2}} \left[ \frac{I_{1}'(\zeta R)}{I_{1}(\zeta R)} + \frac{1}{\zeta R} \right] \mathrm{d}\zeta, \quad x \ll 1$$
(2.14)

where  $\eta = (R - r)(Re_{\lambda}/2x)^{1/2}$ , F satisfies the Blasius equation F''' + FF'' = 0, the prime 243 denotes differentiation,  $\beta = \lim_{\eta \to \infty} (\eta - F) = 1.217..., I_1$  is the modified Bessel function of 244 the first kind, and  $\gamma \in \mathbb{R} < 0$ . Equations (2.9)–(2.11), supplemented by conditions (2.12)– 245 (2.14), are solved by an improved version of the numerical scheme of Hornbeck (1964). A 246 detailed description of the numerical procedure is provided in the supplementary material 247 S1 of Ricco & Alvarenga (2022). The numerical results are discussed in §4.1 of Ricco & 248 Alvarenga (2022). 249

The perturbation-flow unsteady nonlinear boundary-region equations are as follows. 250

The continuity equation is 251

252 
$$\frac{\partial \hat{u}_{m,n}}{\partial \bar{x}} + \frac{\hat{v}_{m,n}}{r} + \frac{\partial \hat{v}_{m,n}}{\partial r} + \frac{im}{r} \hat{w}_{m,n} = 0.$$
(2.15)

The *x*-momentum equation is 254

$$\left(in + \frac{\partial U}{\partial \bar{x}} + \frac{m^2}{\mathcal{F}r^2}\right)\hat{u}_{m,n} + U\frac{\partial \hat{u}_{m,n}}{\partial \bar{x}} + \left(V - \frac{1}{\mathcal{F}r}\right)\frac{\partial \hat{u}_{m,n}}{\partial r} + \hat{v}_{m,n}\frac{\partial U}{\partial r} - \frac{1}{\mathcal{F}}\frac{\partial^2 \hat{u}_{m,n}}{\partial r^2} + \frac{d\hat{\Gamma}_{0,n}}{d\bar{x}} = r_t\hat{X}_{m,n}.$$
(2.16)

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$$\frac{1}{\mathcal{F}}\frac{\partial^2 \hat{u}_{m,n}}{\partial r^2} + \frac{\mathrm{d}\hat{\Gamma}_{0,n}}{\mathrm{d}\bar{x}} = r_t \hat{X}_{m,n}.$$

The *r*-momentum equation is 257

$$\left( in + \frac{\partial V}{\partial r} + \frac{m^2 + 1}{\mathcal{F}r^2} \right) \hat{v}_{m,n} + U \frac{\partial \hat{v}_{m,n}}{\partial \bar{x}} + \hat{u}_{m,n} \frac{\partial V}{\partial \bar{x}} + \left( V - \frac{1}{\mathcal{F}r} \right) \frac{\partial \hat{v}_{m,n}}{\partial r} + \frac{1}{\mathcal{F}} \frac{\partial \hat{p}_{m,n}}{\partial r} - \frac{1}{\mathcal{F}} \frac{\partial^2 \hat{v}_{m,n}}{\partial r^2} + \frac{2im}{\mathcal{F}r^2} \hat{w}_{m,n} = r_t \hat{\mathcal{Y}}_{m,n}.$$

$$(2.17)$$

The  $\theta$ -momentum equation is 260

$$\left(in + \frac{V}{r} + \frac{m^2 + 1}{\mathcal{F}r^2}\right)\hat{w}_{m,n} + U\frac{\partial\hat{w}_{m,n}}{\partial\bar{x}} + \left(V - \frac{1}{\mathcal{F}r}\right)\frac{\partial\hat{w}_{m,n}}{\partial r} + \frac{im}{\mathcal{F}r}\hat{p}_{m,n} - \frac{1}{\mathcal{F}}\frac{\partial^2\hat{w}_{m,n}}{\partial r^2} - \frac{2im}{\mathcal{F}r^2}\hat{v}_{m,n} = r_t\hat{\mathcal{Z}}_{m,n}.$$
(2.18)

261

$$\frac{1}{\mathcal{F}}\frac{\partial^2 \hat{w}_{m,n}}{\partial r^2} - \frac{2im}{\mathcal{F}r^2}\hat{v}_{m,n} = r_t\hat{\mathcal{Z}}_{m,n}.$$

The right-hand sides of the momentum equations (2.16)-(2.18) denote the nonlinear terms 262

$$\begin{aligned}
\hat{X}_{m,n} &= -\left(\frac{\partial \overline{u}\overline{u}}{\partial \overline{x}} + \frac{\partial \overline{u}\overline{v}}{\partial r} + \frac{\overline{u}\overline{v} + im\overline{u}\overline{w}}{r}\right)_{m,n}, \\
\hat{Y}_{m,n} &= -\left(\frac{\partial \overline{u}\overline{v}}{\partial \overline{x}} + \frac{\partial \overline{v}\overline{v}}{\partial r} + \frac{\overline{v}\overline{v} + im\overline{v}\overline{w}}{r}\right)_{m,n}, \\
\hat{Z}_{m,n} &= -\left(\frac{\partial \overline{u}\overline{w}}{\partial \overline{x}} + \frac{\partial \overline{v}\overline{w}}{\partial r} + \frac{im\overline{w}\overline{w}}{r} + \frac{2\overline{v}\overline{w}}{r}\right)_{m,n},
\end{aligned}$$
(2.19)

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where  $\hat{r}$  indicates Fourier transformed quantities. In the limit  $r_t \ll 1$ , the linearised boundaryregion equations of Ricco & Alvarenga (2022) are recovered. The pressure correction  $\hat{\Gamma}_{0,n}$ becomes a further unknown variable for m = 0, and one more condition is thus required to solve the system. Analogous to (2.11) for the base-flow problem, this condition is the conservation of mass flow rate at each instant in time and at each streamwise location. As discussed in Appendix A, this condition is expressed as

270 
$$\int_0^K \hat{u}_{0,n} r dr = 0.$$
 (2.20)

Since the partial differential system (2.15)-(2.20) is parabolic in the streamwise direction and elliptic in the radial and azimuthal directions, appropriate initial and boundary conditions are needed. These conditions are presented in §2.2. Further treatment of (2.15)-(2.20) is carried out in §2.3 for different values of *m*. The numerical procedures are discussed in §2.4.

## 2.2. Initial and boundary conditions

While the streamwise velocity of the induced disturbances acquires an order-one amplitude at  $\bar{x} = O(1)$ , the velocity fluctuations near the pipe inlet are of small amplitude  $O(\epsilon)$  and nonlinear effects can therefore be neglected there. Hence the initial conditions derived by Ricco & Alvarenga (2022) can be used. Comparison of the velocity expansions (2.6) here and (2.6) in Ricco & Alvarenga (2022) leads to the relations

281 
$$\left\{\hat{u}_{m_0,-1}, \hat{v}_{m_0,-1}\right\} = \frac{1}{Re_{\lambda}} \left\{\frac{im_0}{k_x} \bar{u}_x + \bar{u}_x^{(0)}, \frac{im_0}{k_x} \bar{u}_r + \bar{u}_r^{(0)}\right\},$$
(2.21)

where  $\bar{u}_x$ ,  $\bar{u}_r$ ,  $\bar{u}_x^{(0)}$  and  $\bar{u}_r^{(0)}$  are given by the analytical expressions (3.25)–(3.27) and (3.32) in Ricco & Alvarenga (2022). The azimuthal velocity  $\hat{w}_{m_0,-1}$  can be found through the continuity equation (2.15), with  $\hat{u}_{m_0,-1}$  and  $\hat{v}_{m_0,-1}$  given by (2.21). For the opposite wavenumber  $m = -m_0$ , the same streamwise and radial components but opposite azimuthal component are derived

287 
$$\left\{\hat{u}_{-m_0,-1}, \hat{v}_{-m_0,-1}, \hat{w}_{-m_0,-1}\right\} = \left\{\hat{u}_{m_0,-1}, \hat{v}_{m_0,-1}, -\hat{w}_{m_0,-1}\right\}.$$
 (2.22)

288 It also occurs that

$$\hat{u}_{m,n} = \hat{v}_{m,n} = \hat{w}_{m,n} = 0 \quad \text{for } (m,n) \neq (\pm m_0, -1).$$
 (2.23)

Since the streamwise derivative of  $\hat{p}_{m,n}$  is negligible in the *x*-momentum equation (2.16) under the low-frequency assumption, no initial condition for  $\hat{p}_{m,n}$  is required.

In the radial direction, equations (2.15)–(2.20) are subjected to the no-slip and nopenetration conditions at the wall (r = R),

$$\hat{u}_{m,n} = \hat{v}_{m,n} = \hat{w}_{m,n} = 0, \qquad (2.24)$$

while the boundary conditions at the pipe axis (r = 0) are

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## 2.3. Initial-boundary value problems

For convenience of the numerical calculations, the nonlinear boundary-region equations (2.15)-(2.20), together with the initial conditions (2.21)-(2.23) and the boundary conditions (2.24)-(2.25), are solved in different forms according to the value of *m*.

305 *Case I* For the components with  $m \neq 0$ , the pressure  $\hat{p}_{m,n}$  and the azimuthal velocity 306  $\hat{w}_{m,n}$  can be eliminated from (2.15)–(2.19) as in Ricco & Alvarenga (2022). The resulting 307 equations read

$$\left(in + \frac{\partial U}{\partial \bar{x}} + \frac{m^2}{\mathcal{F}r^2}\right)\hat{u}_{m,n} + \left(V - \frac{1}{\mathcal{F}r}\right)\frac{\partial \hat{u}_{m,n}}{\partial r} + U\frac{\partial \hat{u}_{m,n}}{\partial \bar{x}} - \frac{1}{\mathcal{F}}\frac{\partial^2 \hat{u}_{m,n}}{\partial r^2} + \frac{\partial U}{\partial r}\hat{v}_{m,n} = r_t\hat{X}_{m,n},$$
(2.26)

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$$\begin{split} \widehat{V}\hat{v}_{m,n} + \widehat{V}_{r}\frac{\partial\widehat{v}_{m,n}}{\partial r} + \widehat{V}_{x}\frac{\partial\widehat{v}_{m,n}}{\partial\overline{x}} + \widehat{V}_{rr}\frac{\partial^{2}\widehat{v}_{m,n}}{\partial r^{2}} + \widehat{V}_{xr}\frac{\partial^{2}\widehat{v}_{m,n}}{\partial\overline{x}\partial r} + \widehat{V}_{rrr}\frac{\partial^{3}\widehat{v}_{m,n}}{\partial r^{3}} + \widehat{V}_{xrr}\frac{\partial^{3}\widehat{v}_{m,n}}{\partial\overline{x}\partial r^{2}} + \\ \widehat{V}_{rrrr}\frac{\partial^{4}\widehat{v}_{m,n}}{\partial r^{4}} + \widehat{U}\hat{u}_{m,n} + \widehat{U}_{r}\frac{\partial\widehat{u}_{m,n}}{\partial r} + \widehat{U}_{x}\frac{\partial\widehat{u}_{m,n}}{\partial\overline{x}} + \widehat{U}_{rr}\frac{\partial^{2}\widehat{u}_{m,n}}{\partial r^{2}} + \widehat{U}_{xr}\frac{\partial^{2}\widehat{u}_{m,n}}{\partial\overline{x}\partial r} + \\ \widehat{U}_{xrr}\frac{\partial^{3}\widehat{u}_{m,n}}{\partial\overline{x}\partial r^{2}} = r_{t}\frac{r^{2}}{m^{2}}\frac{\partial^{2}\widehat{X}_{m,n}}{\partial\overline{x}\partial r} + r_{t}\widehat{Y}_{m,n} + \frac{ir_{t}}{m}\frac{\partial\left(r\widehat{Z}_{m,n}\right)}{\partial r}, \end{split}$$

$$(2.27)$$

where the coefficients  $\hat{V}, \hat{V}_r, \hat{V}_x, \dots, \hat{U}_{xrr}$  are given in Appendix **B**. Only the initial and boundary conditions for  $\{\hat{u}_{m,n}, \hat{v}_{m,n}\}$  are needed in this case. The initial conditions are given in (2.21)–(2.23). The boundary conditions are

$$\hat{u}_{m,n} = \hat{v}_{m,n} = \hat{v}'_{m,n} = 0, \quad \text{at } r = R$$
 (2.28)

316 and

$$\begin{array}{l}
\hat{u}_{m,n} = 0, \ \hat{v}'_{m,n} = 0, \ \hat{v}''_{m,n} = 0, \quad \text{for} \quad |m| = 1, \\
\hat{u}_{m,n} = 0, \ \hat{v}_{m,n} = 0, \ \hat{v}''_{m,n} = 0, \quad \text{for} \quad |m| = 2, \\
\hat{u}_{m,n} = 0, \ \hat{v}_{m,n} = 0, \ \hat{v}'_{m,n} = 0, \quad \text{for} \quad |m| > 2, \end{array}\right\} \quad \text{at} \ r = 0. \tag{2.29}$$

At the pipe wall, r = R, the last condition  $\hat{w}_{m,n} = 0$  in (2.24) is replaced by  $\hat{v}'_{m,n} = 0$  in (2.28), 318 which is obtained by inserting (2.24) into the continuity equation (2.15). At the pipe axis, 319 r = 0, the conditions for  $\hat{w}$  and  $\hat{w}'$  in (2.25) for different *m* are replaced following the physical 320 constraints proposed by Batchelor & Gill (1962), Khorrami et al. (1989), Tuckerman (1989) 321 and Lewis & Bellan (1990), as discussed in supplementary material S3 of Ricco & Alvarenga 322 (2022). The azimuthal velocity  $\hat{w}_{m,n}$  can be obtained a posteriori from the continuity equation 323 324 and the pressure  $\hat{p}_{m,n}$  can then be calculated from either the r-momentum equation (2.17) or the  $\theta$ -momentum equation (2.18). 325

*Case II* For the components with m = 0, the pressure  $\hat{p}_{0,n}$  appears only in the *r*-momentum equation (2.17). The three velocity components  $\{\hat{u}_{0,n}, \hat{v}_{0,n}, \hat{w}_{0,n}\}$  can be solved by the continuity, *x*- and  $\theta$ -momentum equations,

329 
$$\frac{\partial \hat{u}_{0,n}}{\partial \bar{x}} + \frac{\hat{v}_{0,n}}{r} + \frac{\partial \hat{v}_{0,n}}{\partial r} = 0, \qquad (2.30)$$

$$330 \qquad \left(in + \frac{\partial U}{\partial \bar{x}}\right)\hat{u}_{0,n} + U\frac{\partial \hat{u}_{0,n}}{\partial \bar{x}} + \left(V - \frac{1}{\mathcal{F}r}\right)\frac{\partial \hat{u}_{0,n}}{\partial r} + \hat{v}_{0,n}\frac{\partial U}{\partial r} - \frac{1}{\mathcal{F}}\frac{\partial^2 \hat{u}_{0,n}}{\partial r^2} + \frac{d\hat{\Gamma}_{0,n}}{d\bar{x}} = r_t\hat{X}_{0,n},$$

$$(2.31)$$

331 
$$\left(in+\frac{V}{r}+\frac{1}{\mathcal{F}r^2}\right)\hat{w}_{0,n}+U\frac{\partial\hat{w}_{0,n}}{\partial\bar{x}}+\left(V-\frac{1}{\mathcal{F}r}\right)\frac{\partial\hat{w}_{0,n}}{\partial r}-\frac{1}{\mathcal{F}}\frac{\partial^2\hat{w}_{0,n}}{\partial r^2}=r_t\hat{\mathcal{Z}}_{0,n},\qquad(2.32)$$

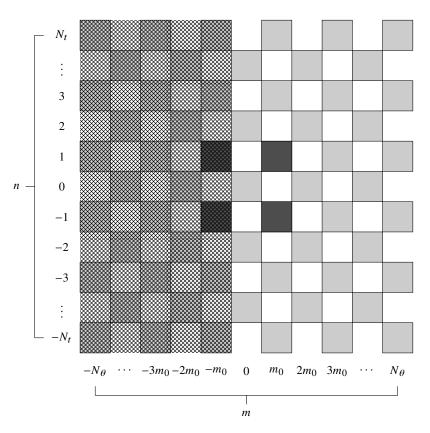


Figure 2: Sketch of Fourier modes induced by a pair of free-stream vortical modes. Dark grey squares: forcing modes  $(\pm m_0, \pm 1)$ . Light grey squares: nonlinearly generated modes. The modes in the shaded area are computed through the Hermitian property (2.8).

together with (2.20) for the conservation of the mass flow rate, as discussed in §2.1. The pressure  $\hat{p}_{0,n}$  is computed *a posteriori* by integrating the *r*-momentum equation (2.17). The boundary conditions for the velocity components and the pressure are given in (2.24) and (2.25) for m = 0. The initial conditions for  $\hat{u}_{0,n}$ ,  $\hat{v}_{0,n}$  are null.

## 336

## 2.4. Numerical procedures

The initial-boundary value problems are solved by marching in the streamwise direction 337  $\bar{x}$ . The governing equations for both cases are discretised by second-order finite-difference 338 schemes employing a one-sided backward uniform grid along  $\bar{x}$  and a central-difference 339 uniform grid along r. The discretised system of case I forms a block tridiagonal matrix and 340 is solved at each  $\bar{x}$  location by a standard block tridiagonal matrix algorithm (Cebeci 2002). 341 For case II, the composite trapezoidal rule is used for the calculation of the integral (2.20). 342 Since the velocity components and the pressure gradient are computed simultaneously, the 343 block tridiagonal structure of the matrix is lost. A novel modified block tridiagonal matrix 344 algorithm is utilised to accelerate the numerical solution of this system, as discussed in 345 Appendix C. 346 The computation of the nonlinear terms on the right-hand sides of the momentum equations 347 is refined by a predictor–corrector method at each  $\bar{x}$  location. In the predictor step, the initial 348

approximation of the nonlinear terms uses the results at the previous  $\bar{x}$  location to treat the discretised nonlinear system explicitly. The velocity computed from the predictor step is used

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351 to improve the initial guess in the corrector step. This iteration is repeated until a convergence criterion is fulfilled. An under-relaxation method is used to accelerate this procedure. At each 352 iteration, nonlinear terms are calculated using the pseudo-spectral method, in which first the 353 Fourier coefficients of the velocity components are transformed to the physical space to carry 354 out the multiplications, and the products are then transformed back to the spectral space. 355 The aliasing error is eliminated by employing the 3/2 rule, which avoids the spurious energy 356 357 cascade from the unresolved high-frequency modes into the resolved low-frequency ones. As the Hermitian property is applied for the azimuthal angle  $\theta$ , only the Fourier modes 358 with non-negative indices m need to be calculated. The modes with negative m indices are 359 evaluated through (2.8). Figure 2 shows a sketch of the Fourier modes induced by a pair 360 of free-steam vortical modes  $(\pm m_0, \pm 1)$ . Only the modes with  $m = \pm m_0, \pm 2m_0, \pm 3m_0, \cdots$ 361 and  $n = \pm 1, \pm 2, \pm 3, \cdots$  can be generated by nonlinearity. Fourier modes are truncated at 362  $m = \pm N_{\theta}$  and  $n = \pm N_t$  for the azimuthal wavenumber and the frequency, respectively. 363 Resolution checks show that the use of  $N_t = 6$ ,  $N_{\theta} = 12$  is sufficient to capture the nonlinear 364 effects induced by the free-stream forcing modes with wavenumber  $m_0 = 2$ . For larger  $m_0$ , a 365 correspondingly larger value of  $N_{\theta}$  is necessary (e.g.  $N_{\theta} = 18$  for  $m_0 = 3$ ). 366

## 367 **3. Results**

In the analysis of the flow, the kinetic energy of the free-stream gust averaged over the pipe cross-section is kept constant:

370 
$$\mathcal{E}_{m_0,l}^{gust} = \frac{1}{2\pi R^2} \int_0^{2\pi} \int_0^R \left( |\tilde{u}|^2 + |\tilde{v}|^2 + |\tilde{w}|^2 \right) r dr d\theta$$

$$4\epsilon^2 \int_0^R \left[ \left( \sum_{m_0,l=0}^{\infty} |I_{m_0}(r_0)|^2 + \left( \hat{v}_{m_0}^{\infty} J_{m_0}(r_0) \right)^2 + \left( \hat{v}_{m_0}^{\infty} J_{m_0}'(r_0) \right)^2 \right] dr d\theta$$
(2.1)

371  
372 
$$= \frac{4\epsilon^2}{R^2} \int_0^R \left[ \left( \hat{u}_{m_0}^{\infty} J_{m_0}(r_0) \right)^2 + \left( \frac{\hat{v}_{m_0}^{\infty} J_{m_0}(r_0)}{r_0} \right)^2 + \left( \frac{\hat{v}_{m_0}^{\infty} J'_{m_0}(r_0)}{m_0} \right)^2 \right] r dr, \quad (3.1)$$

where the gust velocity components in (2.2) have been used. The relation (2.3) is utilised to eliminate  $\hat{w}_{m_0}^{\infty}$  from (3.1). Without losing generality,  $\hat{u}_{m_0}^{\infty}$  is fixed at 1 in our analysis. With m<sub>0</sub> and l specified, the only parameter to be determined is  $\hat{v}_{m_0}^{\infty}$ , which is found by equating  $\mathcal{E}_{m_0,l}^{gust}$  to  $\mathcal{E}_{1,1}^{gust}$ , the perturbation energy for  $m_0 = l = 1$  and  $\hat{v}_{m_0}^{\infty} = 1$ . A similar approach was adopted in Schmid & Henningson (1994), where the maximum energy amplification was computed over initial conditions with the same energy norm. The intensity used to measure the fluctuation level of the gust is defined as  $Tu = \sqrt{(2/3)\mathcal{E}_{m_0,l}^{gust}}$ .

In §2, the circumferential wavelength of the gust  $\lambda^*$  at the pipe radius is selected as the 380 reference length in order to relate our asymptotic analysis to the boundary-layer analysis of 381 Leib et al. (1999), while the numerical results are presented herein with quantities rescaled 382 by the pipe radius  $R^*$ , i.e.  $u = u(x_R, r_R; k_{x,R}, Re_R, l, m_0)$ , where  $x_R = x^*/R^*$ ,  $r_R = r^*/R^*$ , 383  $k_{x,R} = k_x^* R^*$  and  $Re_R = U_{\infty}^* R^* / \nu^*$ . We focus on the nonlinear evolution of disturbances in 384 the parameter space  $k_{x,R} \ll 1$  and  $Re_R < 10000$ , where Tollmien–Schlichting waves are not 385 present (refer to figure 2 of Ricco & Alvarenga (2022)). In our reference case,  $k_{x,R} = 0.02$ , 386  $Re_R = 1000, l = 3, m_0 = 2 \text{ and } \epsilon = 0.05 \text{ (i.e. } Tu \approx 4\%\text{)}.$ 387

The intensity of the disturbances is monitored by the root mean square (r.m.s.) of the streamwise velocity fluctuation,  $u_{rms}$  (Pope 2000, p.687):

$$u_{rms} = r_t \left( \sum_{m=-N_{\theta}}^{N_{\theta}} \sum_{n=-N_t}^{N_t} \left| \hat{u}_{m,n} \right|^2 \right)^{1/2}, \quad n \neq 0.$$
(3.2)

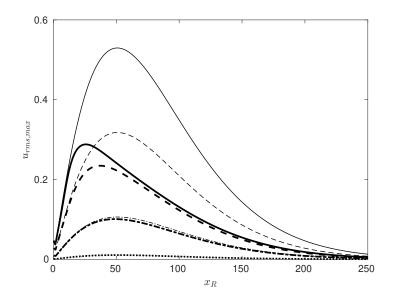


Figure 3: Thick lines: nonlinear streamwise development of  $u_{rms,max}$  for  $\epsilon = 0.001$  (dotted), 0.01 (dash-dotted), 0.03 (dashed), 0.05 (solid). Thin lines: linear solutions rescaled by corresponding  $\epsilon$  value.

## 3.1. Effect of flow parameters

Figure 3 shows the nonlinear streamwise development of the maximum  $u_{rms}$  (thick lines), 392 i.e.  $u_{rms,max} = \max_{r_R} u_{rms}$ , for different values of  $\epsilon = 0.001, 0.01, 0.03, 0.05$  (i.e.  $Tu \approx$ 393 0.08%, 0.8%, 2.4%, 4%). The linear results are rescaled by the corresponding  $\epsilon$  value and 394 displayed by thin lines. The linear and nonlinear solutions overlap when the amplitude 395 of the oncoming disturbance is small ( $\epsilon = 0.001$ ) due to the weak nonlinear interaction, 396 while nonlinear effects become more intense as  $\epsilon$  increases. When  $\epsilon = 0.03$  and 0.05, 397 the nonlinear growth of the disturbances agrees with the corresponding linear growth only 398 near the pipe inlet, and becomes much slower farther downstream. The peak location of 399 the nonlinear profiles moves upstream as  $\epsilon$  increases, and the peak amplitude is lower than 400 401 the corresponding linear one. This latter result indicates the stabilising role of nonlinearity and the overprediction of the linear results. The maximum amplification of the nonlinear 402 solution for  $\epsilon = 0.05$  is, for example, only 54.4% of that of the linear solution. Sufficiently 403 downstream, both linear and nonlinear disturbances experience monotonic decay and tend to 404 zero. The stabilising effect of nonlinearity has already been noticed, for example, by Ricco 405 et al. (2011) and Marensi & Ricco (2017) for the development of the streaks in boundary 406 layers over flat and concave plates, respectively. 407

Figure 4 shows the effects of different parameters,  $k_{x,R}$ ,  $Re_R$ , l and  $m_0$ , on the nonlinear development of  $u_{rms,max}$  along the streamwise direction  $x_R$ . In figure 4(*a*), the overlap of profiles at the smaller  $x_R$  indicates that the streamwise wavenumber  $k_{x,R}$  has no influence on the initial growth of the disturbances. The profiles for  $k_{x,R} = 0.001$  and 0.02 are almost indistinguishable for the whole extent  $x_R$  of the pipe. By further increasing  $k_{x,R}$  up to 0.1, the amplitude of  $u_{rms,max}$  reaches a lower peak and decays at a larger rate.

Figure 4(*b*) displays the influence of the Reynolds number  $Re_R$  ranging from 1000 to 2500. The independence of the initial growth of the disturbance is also found by changing  $Re_R$ . For  $Re_R \leq 2000$ , the evolution features one maximum after the initial growth, while, for  $Re_R > 2000$ , two maxima are observed. Farther downstream, the disturbance decays at a slower rate as  $Re_R$  increases.

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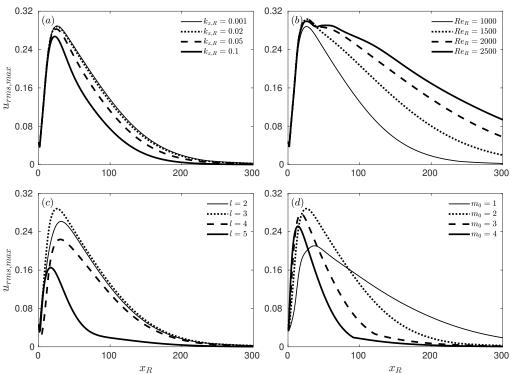


Figure 4: Effects of different parameters on the streamwise development of  $u_{rms,max}$ . (a) Streamwise wavenumber  $k_{x,R}$ ; (b) Reynolds number  $Re_R$ ; (c) parameter l characterising the radial length scale; (d) azimuthal wavenumber  $m_0$ .

Figure 4(*c*) shows how the change of the parameter *l* affects the downstream development of  $u_{rms,max}$ . As the characteristic radial scale of the oncoming disturbances is defined by the *l*th zero of the Bessel function, i.e.  $\xi_{m_0,l}$  in expansion (2.1)–(2.2), a large *l* value corresponds to a small characteristic radial length scale, as shown in figure 20(*a*) of Ricco & Alvarenga (2022) The most intense growth occurs for l = 3.

The effect of the azimuthal wavenumber  $m_0$  is shown in figure 4(d). Increasing  $m_0$  induces a more intense initial growth. Different from the linear case where the maximum growth is found at wavenumber  $m_0 = 3$  (Ricco & Alvarenga 2022), the nonlinear disturbances grow the most for  $m_0 = 2$ . A similar finding was reported by Reshotko & Tumin (2001) in the analysis of spatial transient growth in fully developed pipe flow, where non-stationary optimal disturbances were obtained for azimuthal wavenumbers larger than 1. The smaller  $m_0$ , the more the disturbances persist downstream.

## 3.2. *Results for a representative case*

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The representative case with  $k_{x,R} = 0.02$ ,  $Re_R = 1000$ , l = 3,  $m_0 = 2$ ,  $\epsilon = 0.05$  is analysed. 432 Figures 5(a) and 5(b) show the profiles of  $u_{rms}$  at different streamwise locations. The 433 maximum of  $u_{rms}$  appears close to the wall for locations near the pipe inlet, and gradually 434 shifts towards the centreline as  $x_R$  increases. Its amplitude increases with  $x_R$  up to  $x_R \approx 26$ , 435 after which a monotonic decrease occurs downstream. Near the pipe inlet, a significant 436 disturbance growth is obtained in the region close to the pipe core  $(0.1 < r_R < 0.5)$  where 437 438 the base flow is largely inviscid. The disturbances in boundary layers subjected to free-stream turbulence show a similar growth in the outer region (figure 2(c) of Matsubara & Alfredsson 439

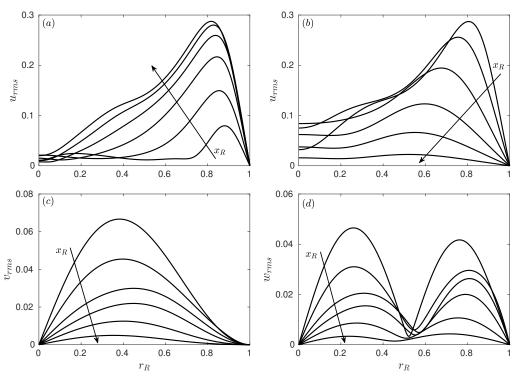


Figure 5: Profiles of  $u_{rms}$ ,  $v_{rms}$  and  $w_{rms}$  at different streamwise locations: (a) growing  $u_{rms}$  at  $x_R = 4, 8, 12, 16, 20, 24$ ; (b) decaying  $u_{rms}$  at  $x_R = 28, 44, 70, 104, 140, 191$ . (c, d)  $v_{rms}$  and  $w_{rms}$  at  $x_R = 4, 12, 20, 28, 44, 70$ . Arrows indicate the increasing  $x_R$  direction.

440 (2001) and figure 10 of Ricco *et al.* (2011)). This growth does not occur in the linearised case, 441 where the disturbances are confined in the near-wall region (figure 15 of Ricco & Alvarenga 442 (2022)). The streamwise developments of  $v_{rms}$  and  $w_{rms}$  are shown in figures 5(c) and 5(d). 443 The amplitudes of  $v_{rms}$  and  $w_{rms}$  are comparable with that of  $u_{rms}$  close to the pipe inlet, 444 while they become much smaller downstream after considerable attenuation.

Figure 6 displays the downstream development of the forcing mode (m, n) = (2, 1) (red 445 line) and the nonlinearly generated modes, which are characterised by  $\max_{r_R} |r_t \hat{u}_{m,n}|$ , the 446 maximum intensity of  $|r_t \hat{u}_{m,n}|$  at each  $x_R$  location. For the assumed free-stream disturbances 447 (2.1), modes (m, n) and (-m, n) have the same amplitude. Modes (m, n) and (-m, -n) also 448 have the same amplitude because of the Hermitian property (2.8). Therefore, without losing 449 generality, only the results for  $m \ge 0$  and  $n \ge 0$  are presented. The mean-flow distortion  $\hat{u}_{0,0}$ 450 acquires considerable growth shortly downstream of the pipe inlet, overshoots the forcing 451 mode  $\hat{u}_{2,1}$  at  $x_R \approx 24.4$ , and becomes dominant downstream. The amplitude of the higher 452 harmonics also grows because of the strong nonlinear interaction when  $\epsilon = 0.05$ , and then 453 attenuates due to viscous effects. Downstream of  $x_R = 200$ , only the forcing mode  $\hat{u}_{2,1}$ , the 454 mean-flow distortion  $\hat{u}_{0,0}$  and the pulsatile mode  $\hat{u}_{0,2}$  still exist. They all decay to zero farther 455 downstream. 456

Figure 7 shows the streamwise velocity profiles of the mean-flow distortion  $r_t \hat{u}_{0,0}$ , the forcing modes  $r_t |\hat{u}_{2,1}|$  and the higher harmonics  $r_t |\hat{u}_{0,2}|$ ,  $r_t |\hat{u}_{4,0}|$ ,  $r_t |\hat{u}_{4,2}|$  at six different streamwise locations,  $x_R = 4, 16, 32, 51, 96, 180$ . The most intense growth is obtained by max<sub>r<sub>R</sub></sub> | $r_t \hat{u}_{0,0}$ | at  $x_R = 51$  (refer to figure 6). The ordinate axis in 7(*a*) and 7(*f*) is stretched

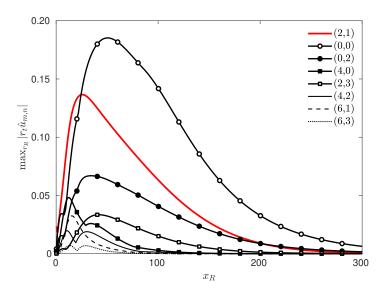


Figure 6: Streamwise development of the forcing mode (red line) and nonlinearly generated modes, characterised by  $\max_{r_R} |r_t \hat{u}_{m,n}|$ .

by a factor of 2 for clarity. Significant growth and decay in the velocity amplitude are observed for modes  $r_t \hat{u}_{0,0}, r_t |\hat{u}_{2,1}|$  and  $r_t |\hat{u}_{0,2}|$  along the pipe entrance. Moreover, the shape of velocity profiles changes substantially as the flow evolves downstream. The positive values of the mode  $r_t \hat{u}_{0,0}$  near the wall indicate an increase of the wall-shear stress. The second harmonics,  $r_t |\hat{u}_{4,0}|$  and  $r_t |\hat{u}_{4,2}|$ , experience considerable attenuation shortly after the initial growth and are almost negligible at  $x_R = 96$  and 180.

Figure 8 shows the streamwise velocity profiles of the laminar base flow U (dashed lines) 467 and the mean flow  $\bar{U}$  (solid lines), i.e. the velocity averaged in t and  $\theta$ , at the same streamwise 468 locations as those in figure 7. Mathematically, the distorted mean flow  $\overline{U}$  is the sum of the 469 laminar base flow and the mean-flow distortion, i.e.  $\bar{U} = U + r_t \hat{u}_{0,0}$ . A significant deviation 470 from the laminar base flow is observed in figure  $8(d) (x_R = 51)$ , where  $\max_{r_R} |r_t \hat{u}_{0,0}|$  reaches 471 the maximum growth. In the pipe core region, the profile exhibits a deficit with respect to 472 473 the laminar base flow, while it is larger than the laminar value near the wall. The profiles of 474 the mean-flow distortion  $r_t \hat{u}_{0,0}$  shown in figure 7 further explain these velocity deficits and surpluses. Positive mean-flow distortion  $r_t \hat{u}_{0,0}$  always exists near the pipe wall, while in the 475 pipe core it is positive only near the inlet, and negative farther downstream. 476

Figure 9 displays contour plots of the velocity components  $\tilde{u}$ ,  $\tilde{v}$  and  $\tilde{w}$  (from left to right) at 477  $\bar{t} = 0$  and four different streamwise locations  $x_R = 4, 26, 60, 150$  (from top to bottom). These 478 plots visualise the formation and evolution of elongated pipe-entrance nonlinear structures 479 (EPENS). Near the pipe inlet ( $x_R = 4$ ), the three velocity components are of comparable 480 amplitude. The EPENS appear because the streamwise component  $\tilde{u}$  becomes prevalent at 481  $x_R = 26$  (attributed to the growth of  $\tilde{u}$  and the attenuation of  $\tilde{v}$  and  $\tilde{w}$ ), where the disturbances 482 are most amplified, as shown in figure 3. In contrast to the nonlinear streaks observed in 483 transitional boundary-layer flows (Matsubara & Alfredsson 2001) that are confined in the 484 near-wall region, these EPENS occupy the entire cross-section with two high-speed streaks 485 near the pipe wall, and two low-speed streaks near the pipe core. The twofold rotational 486 symmetry featured by these EPENS results from the dominance of the forcing mode  $\hat{u}_{2,1}$ 487 488 among all the modes with  $m \neq 0$  (refer to figure 6). The modes with m = 0 are uniform in the azimuthal direction. The gradual downstream attenuation after  $x_R = 26$  can be observed 489

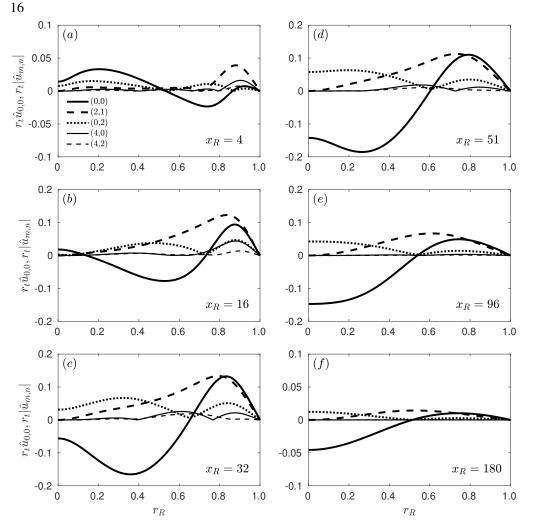


Figure 7: Streamwise velocity profiles of the mean-flow distortion  $r_t \hat{u}_{0,0}$ , forcing modes  $r_t |\hat{u}_{2,1}|$  and second harmonics  $r_t |\hat{u}_{0,2}|$ ,  $r_t |\hat{u}_{4,0}|$ ,  $r_t |\hat{u}_{4,2}|$  at different streamwise locations.

in the last two rows of figure 9, corresponding to  $x_R = 60$  and 150. At  $x_R = 60$  and 150, the low-speed streaks merge near the pipe core, flanked by the high-speed streaks on their sides. Contours of the streamwise velocity  $\tilde{u}$  at  $x_R = 200$  and four different time phases  $\bar{t} = 0, \pi/4, \pi/2, 3\pi/4$  are shown in figure 10. The radial and azimuthal velocities  $\tilde{v}$  and  $\tilde{w}$  are  $O(10^{-5})$  at that location, thus are not shown. The distributions of  $\tilde{u}$  at  $\bar{t} \in [\pi, 2\pi]$  exhibit the same features as those at  $\bar{t} \in [0, \pi]$ , but with a rotation of 90° around the pipe axis.

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## 3.3. Comparison with travelling waves

The nonlinear vortical structures evolving along the pipe entrance are now compared with travelling waves appearing in fully developed pipe flow. Inspired by the self-sustained process proposed by Waleffe (1997), Faisst & Eckhardt (2003) and Wedin & Kerswell (2004) discovered three-dimensional travelling waves (TWs) in pipe flow. These nonlinear waves consist of streamwise vortices, streaks and streamwise-dependent wavy structures. They were also observed experimentally in turbulent puffs and in fully developed turbulence by Hof *et al.* (2004). New families of TWs have also been reported in Pringle & Kerswell

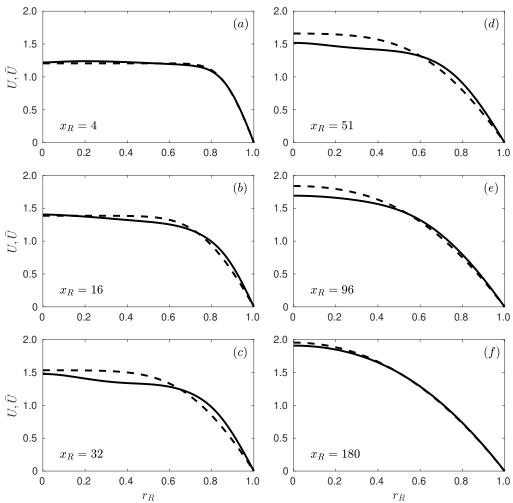


Figure 8: Streamwise velocity profiles of the laminar base flow U (dashed line) and the distorted mean flow  $\overline{U} = U + r_t \hat{u}_{0,0}$  (solid line) at different streamwise locations.

(2007) and Pringle *et al.* (2009). These TWs are nonlinear solutions of the Navier–Stokes
equations and they capture distinct features of coherent structures observed in turbulent pipe
flow (Graham & Floryan 2021). Willis & Kerswell (2008) suggested that these TWs populate
an intermediate region between the laminar and turbulent states in phase space. However,
the physical origin of these TWs has not been discussed and remains unclear.

As shown in figure 11, excellent visual agreement occurs between the  $\mathcal{R}_3$ -TW (where 509  $\mathcal{R}_h$  represents the h-fold rotational symmetry) found by Wedin & Kerswell (2004) and the 510  $\mathcal{R}_3$ -EPENS at the same Reynolds number,  $Re_R = 900$ . (The Reynolds number based on the 511 pipe diameter used in Wedin & Kerswell (2004), Willis et al. (2017) and Kerswell & Tutty 512 (2007) has been converted to  $Re_R$  herein.) The EPENS are shown at  $x_R = 18$  and  $\bar{t} = 0$ , 513 where  $u_{urm,max}$  attains the largest amplitude. Remarkable agreement is observed for the 514 streamwise vortices and the high/low-speed streaks, although the TWs are found in fully 515 developed pipe flow while the EPENS exist in the pipe entrance region. Both the  $\mathcal{R}_3$ -TW 516 517 and  $\mathcal{R}_3$ -EPENS have three equispaced low-speed streaks (dark) located towards the centre and three equispaced high-speed streaks (light) positioned near the wall. For both sets of 518

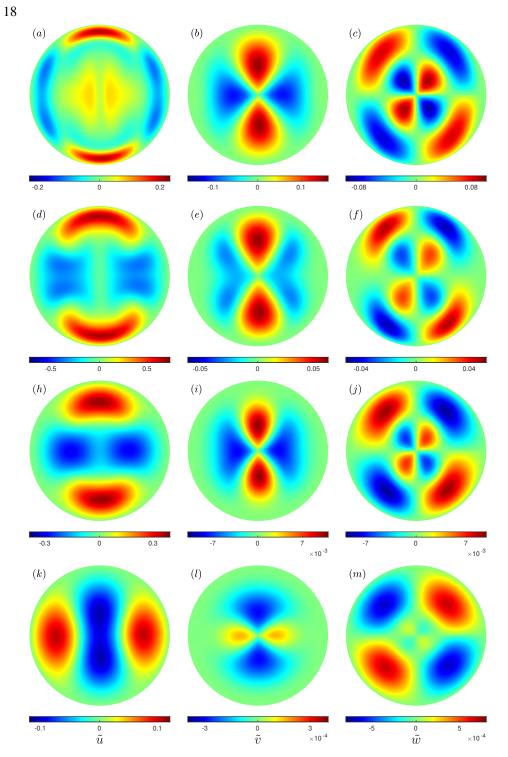


Figure 9: Contours of the velocity components  $\tilde{u}$ ,  $\tilde{v}$  and  $\tilde{w}$  (from left to right) at the time instant  $\bar{t} = 0$  and four different locations  $x_R = 4, 26, 60, 150$  (from top to bottom), where the red/blue coloured shading indicates velocity faster/slower than the laminar base-flow velocity *U*. The same shading is used in figure 10.

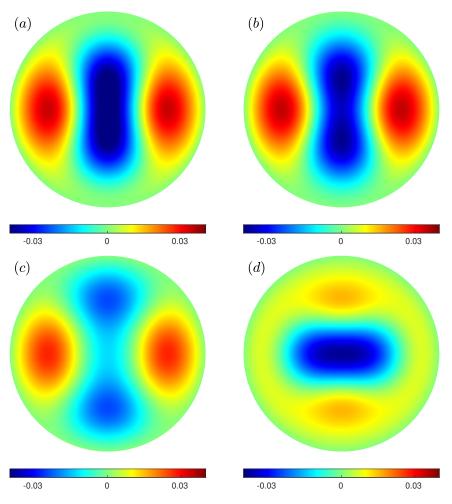


Figure 10: Contours of the streamwise velocity  $\tilde{u}$  at the streamwise location  $x_R = 200$  and four different time phases (a)  $\bar{t} = 0$ , (b)  $\bar{t} = \pi/4$ , (c)  $\bar{t} = \pi/2$ , and (d)  $\bar{t} = 3\pi/4$ .

nonlinear structures, streamwise vortices are located between adjacent low-speed and highspeed streaks, moving fluid towards the pipe axis in correspondence with low-speed streaks
and wallward where high-speed streaks exist.

The TWs originate mathematically from saddle-node bifurcations and are calculated using 522 a homotopy approach. However, this numerical method does not explain the physical origin of 523 TWs. The method to compute the EPENS instead describes the physical origin of EPENS, i.e. 524 the EPENS arise from the algebraic growth, nonlinear interactions and streamwise stretching 525 of realistic vortical disturbances convected by the uniform flow approaching and entering the 526 pipe inlet. We note that other receptivity mechanisms, such as wall vibration or roughness, 527 could also create them. Wedin & Kerswell (2004) found that multiple solution branches 528 coexist at higher Reynolds numbers (refer to figure 10 of Wedin & Kerswell (2004)). Besides 529 the  $\mathcal{R}_h$  solution shown in figure 11(a), which consists of h high-speed streaks near the wall, 530 Wedin & Kerswell (2004) also discovered solutions with 2h near-wall high-speed streaks in 531 other branches. Only EPENS with h high-speed streaks are instead found in our computations. 532 533 With figure 11(b) as a reference, computations of EPENS for  $m_0 = 3$  are carried out for different  $Re_R$ ,  $k_{x,R}$  and l. The results are displayed in figure 12 at the locations where the 534

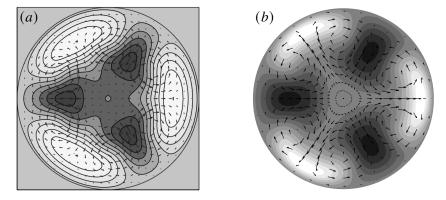


Figure 11: Comparison of velocity fields between the  $\mathcal{R}_3$ -TW and  $\mathcal{R}_3$ -EPENS for  $Re_R = 900$ . The cross-section vectors  $\tilde{v} \mathbf{j} + \tilde{w} \mathbf{k}$  (where  $\mathbf{j}$  and  $\mathbf{k}$  are unit vectors in the radial and azimuthal directions) are indicated by arrows. The streamwise velocity  $\tilde{u}$  is indicated by the shading, where light/dark colour indicates  $\tilde{u}$  faster/slower than the laminar base-flow velocity U. The same shading is used in figures 12, 13 and 14. (*a*) The  $\mathcal{R}_3$ -TW found by Wedin & Kerswell (2004). (*b*) The  $\mathcal{R}_3$ -EPENS calculated at  $x_R = 18$ , where they are most amplified, and  $\bar{t} = 0$  with  $\epsilon = 0.05$ ,  $k_{x,R} = 0.02$ , l = 3 and  $m_0 = 3$ .

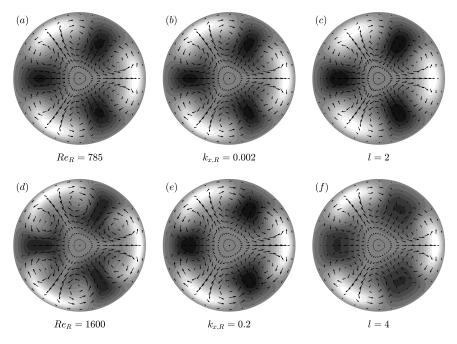


Figure 12: Velocity fields of  $\mathcal{R}_3$ -EPENS at locations where they are most amplified and  $\bar{t} = 0$  for different  $Re_R$ ,  $k_{x,R}$  and l. Unless otherwise stated, the parameters are  $\epsilon = 0.05$ ,  $Re_R = 900$ ,  $k_{x,R} = 0.02$ , l = 3 and  $m_0 = 3$ . (a)  $Re_R = 785$ ,  $x_R = 17$ . (b)  $k_{x,R} = 0.002$ ,  $x_R = 18$ . (c) l = 2,  $x_R = 22$ . (d)  $Re_R = 1600$ ,  $x_R = 19$ . (e)  $k_{x,R} = 0.2$ ,  $x_R = 15$ . (f) l = 4,  $x_R = 20$ .

EPENS are most amplified. Figure 11(*a*) corresponds to solution *a* in figure 10 of Wedin & Kerswell (2004), which was used for the branch continuation. This branch was traced down to  $Re_R = 785$  and up to  $Re_R = 1600$ . Figures 12(*a*) and 12(*d*) show the EPENS calculated at these two Reynolds numbers. The similarities in the dominant streaks and vortices of

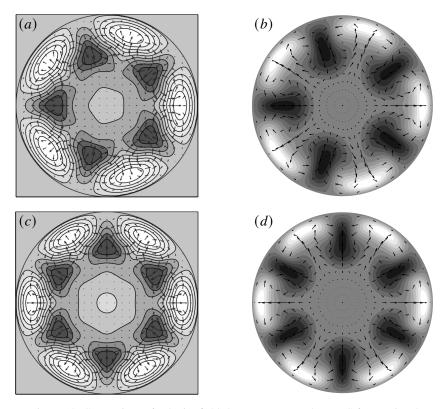


Figure 13: Comparison of velocity fields between TWs and EPENS for rotational symmetries  $\mathcal{R}_5$  at  $Re_R = 1242.75$  and  $\mathcal{R}_6$  at  $Re_R = 1434.5$ . (a, c) The  $\mathcal{R}_5$ - and  $\mathcal{R}_6$ -TW found by Wedin & Kerswell (2004) at their saddle-node bifurcations. (b, d) The  $\mathcal{R}_5$ - and  $\mathcal{R}_6$ -EPENS calculated at  $x_R = 12$  and 11, where they are most amplified, and  $\bar{t} = 0$  for  $\epsilon = 0.05$ ,  $k_{x,R} = 0.02$ , l = 3, and  $m_0 = 5, 6$ .

EPENS for different  $Re_R$  are observed. As  $Re_R$  increases, the low-speed streaks appear 539 slightly narrower along the azimuthal direction, and the high-speed streaks become slightly 540 more flattened towards the wall. The close resemblance among TWs pertaining to the same 541 branch for different  $Re_R$  was also reported in Wedin & Kerswell (2004). Figures 12(b) and 542 12(e) show that varying the frequency by one hundred times has only a minimal impact on 543 the EPENS. The robustness of the EPENS is further confirmed in figures 12(b) and 12(e)544 by varying the radial modulation of the inlet perturbation flow, given by the change of the 545 546 parameter l. Increasing l, indicating an inlet perturbed flow with a smaller radial length scale, has only a mild influence on the EPENS. This result proves that the EPENS are likely to be 547 a strong attractor of the dynamical system. 548

Except for the  $\mathcal{R}_3$  symmetry, only TWs at their saddle-node bifurcations are presented for 549 other rotational symmetry in Wedin & Kerswell (2004). Among these solutions,  $\mathcal{R}_{5}$ - and 550  $\mathcal{R}_6$ -TWs consist of h high-speed streaks near the wall, while  $\mathcal{R}_1$ -,  $\mathcal{R}_2$ - and  $\mathcal{R}_4$ -TWs have 551 2h high-speed streaks. Remarkable agreement between TWs and EPENS is also obtained 552 for the  $\mathcal{R}_5$  and  $\mathcal{R}_6$  rotational symmetries, as reported in figure 13. The EPENS with h-553 fold rotational symmetry observed downstream is always excited by free-stream vortical 554 disturbances with azimuthal wavenumber  $m_0 = h$ . The discovery of  $\mathcal{R}_1$ -TWs, which possess 555 no discrete rotational symmetry, was reported in Pringle & Kerswell (2007). These TWs 556 557 are more important than the rotationally symmetric ones because the upper/lower branches correspond to much higher/lower wall-shear stress values compared to rotationally symmetric 558

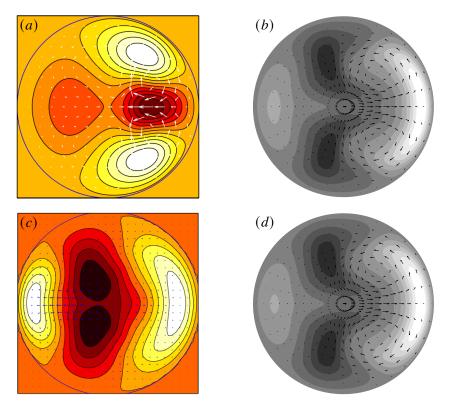


Figure 14: Comparison of velocity fields between the asymmetric TWs and  $\mathcal{R}_1$ -EPENS for  $Re_R = 1450$  (*a*, *b*) and 1340 (*c*, *d*). (*a*, *c*) The asymmetric TWs found by Pringle & Kerswell (2007) and Willis *et al.* (2017), where the white/dark coloured shading indicates  $\tilde{u}$  faster/slower than the laminar base-flow velocity *U*. (*b*, *d*) The  $\mathcal{R}_1$ -EPENS calculated at  $x_R = 36$ , where they are most amplified, and  $\bar{t} = 0$  with  $\epsilon = 0.05$ ,  $k_{X,R} = 0.02$ , l = 3, and  $m_0 = 1$ .

ones. Figure 14(a) shows the velocity field of an asymmetric TW of these new families. One 559 560 low-speed streak is centred at half the distance between the wall and the centreline, and is surrounded by two high-speed streaks. As shown in figure 14(b), rotationally asymmetric 561 EPENS are also found in our calculation when  $m_0 = 1$ . However, they consist of one wide 562 near-wall high-speed streak flanked by two low-speed streaks, and one low-intensity high-563 speed streak on the opposite side of the wide high-speed streak. The cross-section velocity 564 vector field reveals that counter-rotating streamwise vortices occur between the high-speed 565 and the low-speed streaks. Using a feedback control strategy, a new asymmetric TW was 566 identified by Willis *et al.* (2017) (figure 14(c)). Good agreement is noted between the streaks 567 of their TW and our  $\mathcal{R}_1$ -EPENS at the same Reynolds number, whereas only very weak 568 streamwise vortices are found between the wide high-speed streak and low-speed streaks in 569 their case. 570

The comparison of streamwise velocity isosurfaces of the  $\mathcal{R}_3$ -TW calculated by Kerswell & Tutty (2007) and the  $\mathcal{R}_3$ -EPENS at  $Re_R = 1200$  is also very good, as shown in figure 15, where the light and dark shadings denote the streamwise velocity for  $\tilde{u} = 0.3U$  and -0.3U. The  $\mathcal{R}_3$ -TW is displayed versus its wavelength (the diameter of the pipe is used as a reference

<sup>575</sup> length), while the  $\mathcal{R}_3$ -EPENS is displayed for  $13 < x_R < 17$ . Along these distances, both the

576 near-wall high-speed streaks and the low-speed streaks near the pipe core for both the TW

577 and EPENS evolve slowly in the streamwise direction.

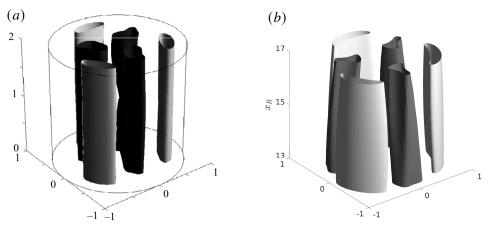


Figure 15: Comparison of streamwise velocity isosurfaces between the  $\mathcal{R}_3$ -TW and  $\mathcal{R}_3$ -EPENS for  $Re_R = 1200$ . The light and dark shading represents the streamwise velocity  $\tilde{u}$  that equals 0.3U and -0.3U. (a) The  $\mathcal{R}_3$ -TW over the wavelength found by Kerswell & Tutty (2007). (b) The  $\mathcal{R}_3$ -EPENS calculated for  $13 \ll x_R \ll 17$  and  $\bar{t} = 0$  with  $\epsilon = 0.05$ ,  $k_{x,R} = 0.2$ , l = 3 and  $m_0 = 3$ .

578 Considering the richness of the phase space, further comparison between TWs and EPENS 579 for different parameters are warranted to fully understand their connection. One challenge in 580 searching for an TW is the daunting numerical process required to find a good initial guess, 581 whereas EPENS can be calculated much more rapidly using our approach. It is therefore 582 suggested that EPENS could be used as initial guesses in the search for TWs.

#### 583

## 3.4. Comparison with experimental data

Ricco & Alvarenga (2022) compared their linearised numerical results to the experimental 584 measurements by Wygnanski & Champagne (1973). For both the mean and perturbation flow, 585 excellent agreement was obtained at a low level of free-stream turbulence intensity, while 586 a significant deviation between the linear results and the experimental data was reported 587 for higher intensities. In figure 16, the experimental data at high turbulence intensity are 588 589 compared with our nonlinear results. The turbulence intensity was measured by  $(u_{rms}/\bar{U})_{cl}$ in Wygnanski & Champagne (1973), where the subscript cl refers to the value at the pipe axis. 590 The values of  $(u_{rms}/\bar{U})_{cl} = 5.8\%$  and 7.8% in Wygnanski & Champagne (1973) are found 591 to be equivalent to  $\epsilon = 0.082$  and 0.12 in our calculation for the case with  $k_{x,R} = 0.118$ , 592 l = 2 and  $m_0 = 2$ . Figure 16(a) shows the good agreement in the mean-flow velocity 593 594 profiles except in the near-wall region where the numerical calculations underpredict the experimental data. Good agreement also occurs in the comparison of the perturbation-flow 595 velocity profiles, as shown in figure 16(b). In Ricco & Alvarenga (2022), the velocity profile 596 was instead predicted by the linearised boundary-region equations to be zero at the pipe axis. 597 The finite perturbations near the pipe axis are well predicted when the nonlinear interactions 598 (i.e.  $r_t \hat{u}_{0,0}$ ) are taken into account. Both studies show the same trend: as the turbulent intensity 599 increases, a larger peak is reached, and the peak position moves towards the wall. The peak 600 of the profiles measured by Wygnanski & Champagne (1973) is obtained at a lower value and 601 located closer to the wall compared to our calculations. The disagreements are likely to come 602 from the different inflows at the pipe inlet. In experiments, the disturbances were generated 603 by an orifice plate or a circular disk placed at the inlet, and no precise information about 604 605 the resulting initial flow was given. The analytical expression (2.1) is instead used to model the vortical disturbances in our calculations. As the flow is described by an initial-boundary 606

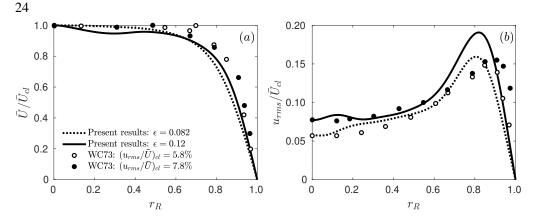


Figure 16: Comparison of (*a*) the mean flow and (*b*) the perturbation flow between the experimental measurements (circles) and present numerical results (lines) for  $Re_R = 1200$  at  $x_R = 30$ . Open and solid circles: experimental data measured by Wygnanski & Champagne (1973) (refer to as WC73 in the figure) with  $(u_{rms}/\bar{U})_{cl} = 5.8\%$  and 7.8%. Dotted and solid lines: present results with  $\epsilon = 0.082, 0.12, k_{x,R} = 0.118, l = 2$  and  $m_0 = 2$ .

value problem in the pipe entrance, the inflow characteristics are crucial for an accurate prediction of the downstream development of the flow.

## 609 4. Summary and conclusions

As a step towards understanding the laminar-turbulent transition in pipe flow, we have 610 investigated the nonlinear evolution of free-stream vortical disturbances entrained in the 611 entrance region of a circular pipe by using a high Reynolds number asymptotic approach. The 612 oncoming disturbances are modelled by a pair of vortical modes with the same frequency but 613 opposite azimuthal wavenumber. A long-wavelength hypothesis is utilised. This hypothesis is 614 inspired by the experimental finding that streamwise-elongated streaks induced by free-stream 615 disturbances in boundary layers amplify significantly (Matsubara & Alfredsson 2001). The 616 disturbance amplitude is assumed to be intense enough for nonlinear interactions to occur. 617 618 The present study can therefore be viewed as an extension of Ricco & Alvarenga (2022) to the nonlinear case. 619

The resultant nonlinear system is solved numerically by a marching procedure in the 620 streamwise direction. A parametric study reveals the stabilising effect of nonlinearity on the 621 intense algebraic disturbance growth near the pipe inlet. The linear theory thus overpredicts 622 the nonlinear disturbance intensity. The effect of the Reynolds number, the streamwise and 623 azimuthal wavelengths, and the radial length scale of the inlet disturbance on the nonlinear 624 625 evolution of the disturbances is investigated. The mean-flow distortion  $\hat{u}_{0,0}$  grows significantly shortly downstream of the pipe inlet, being negative in the pipe core and positive near the 626 wall, indicating an increase of wall-shear stress. 627

We report the formation, amplification and attenuation of rotationally symmetric elongated 628 pipe-entrance nonlinear structures (EPENS). The distinct features of  $\mathcal{R}_h$ -EPENS (h > 1) are 629 equispaced h high-speed streaks around the pipe wall and h low-speed streaks in the pipe core. 630 A remarkable resemblance between these structures and nonlinear travelling waves (TWs) 631 occurring in fully developed pipe flow is noted for  $m_0 = 3, 5, 6$ . Rotationally asymmetric 632 EPENS are discovered for  $m_0 = 1$ . They also agree well with asymmetric TWs for  $m_0 = 1$ . 633 634 These similarities may shed light on the physical origin of nonlinear TWs. The robustness of the EPENS in response to changes of different inlet flow conditions is demonstrated, 635

indicating that the EPENS are likely to be a strong attractor of the dynamical system. We
also suggest the potential use of EPENS as an initial guess in the numerical search for the
nonlinear TWs. More investigations are necessary to clarify the connection between the
EPENS and the TWs.

With the inclusion of nonlinear effects, good agreement between our calculations and the experimental measurements of Wygnanski & Champagne (1973) is obtained for both the mean flow and the perturbation flow. Further improvement may be gained by using a continuous spectrum of free-stream disturbances as oncoming disturbances. Performing a secondary instability analysis of the EPENS is also of interest. The EPENS attenuate downstream in our calculation, but they may persist when the growth of small-amplitude secondary disturbances is taken into account.

It is our hope that the theoretical work presented herein will motivate more direct numericalsimulations and experimental investigations in the entrance region of pipe flow.

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654 Declaration of interests. The authors report no conflict of interest.

## 655 Appendix A. Conservation of the mass flow rate

656 At each instant in time and at each streamwise location, the mass flow rate is conserved.

Since the flow is incompressible, this condition translates to the conservation of the bulk velocity, i.e. the streamwise velocity averaged on the cross-section of the pipe is equal to the opcoming velocity  $U^*$ :

659 oncoming velocity  $U_{\infty}^*$ :

660 
$$\frac{1}{\pi R^2} \int_0^{2\pi} \int_0^R (U + r_t \bar{u}) \, r dr d\theta = 1.$$
 (A1)

Substituting (2.7) into (A 1), equation (2.11) is obtained for the laminar base flow and

662 
$$\sum_{m,n=-\infty}^{\infty} \int_0^{2\pi} \int_0^R \hat{u}_{m,n} e^{im\theta + in\bar{t}} r dr d\theta = 0.$$
(A 2)

 $_{663}$  By using the orthogonality property of the Fourier series, equation (2.20) is obtained, which is

the condition needed to solve the system because the pressure  $\Gamma_{0,n}$  is an additional unknown.

## 665 Appendix B. Coefficients of equation (2.27)

The expressions of  $\{\widehat{V}, \widehat{V}_r, \widehat{V}_x, \cdots, \widehat{U}_{xrr}\}$  in equation (2.27) are

$$\begin{split} \widehat{V} &= \left(1 - \frac{1}{m^2}\right) \left(in + \frac{\partial V}{\partial r} + \frac{m^2 - 1}{\mathcal{F}r^2}\right) + \frac{2r}{m^2} \frac{\partial^2 U}{\partial \bar{x} \partial r} + \frac{r^2}{m^2} \frac{\partial^3 U}{\partial \bar{x} \partial r^2}, \\ \widehat{V}_r &= \left[ \left(1 - \frac{4}{m^2}\right) V - \frac{3r}{m^2} \left(in + \frac{\partial V}{\partial r}\right) - \left(2 + \frac{1}{m^2}\right) \frac{1}{\mathcal{F}r} \right] + \frac{r^2}{m^2} \frac{\partial^2 U}{\partial \bar{x} \partial r}, \\ \widehat{V}_x &= \left(1 - \frac{1}{m^2}\right) U + \frac{r}{m^2} \left(\frac{\partial U}{\partial r} + r \frac{\partial^2 U}{\partial r^2}\right), \end{split}$$

$$\begin{split} \widehat{V}_{rr} &= -\left[\frac{r}{m^2}\left(inr+5V+r\frac{\partial V}{\partial r}\right) + \left(2-\frac{5}{m^2}\right)\frac{1}{\mathcal{F}}\right],\\ \widehat{V}_{xr} &= -\frac{3Ur}{m^2},\\ \widehat{V}_{rrr} &= -\frac{r}{m^2}\left(rV-\frac{6}{\mathcal{F}}\right),\\ \widehat{V}_{xrr} &= -\frac{r^2U}{m^2},\\ \widehat{V}_{rrrr} &= \frac{r^2}{m^2\mathcal{F}},\\ \widehat{U} &= \frac{\partial V}{\partial \bar{x}} + \frac{2r}{m^2}\frac{\partial^2 U}{\partial \bar{x}^2} + \frac{r^2}{m^2}\frac{\partial^3 U}{\partial \bar{x}^2 \partial r},\\ \widehat{U}_r &= \frac{r}{m^2}\frac{\partial V}{\partial \bar{x}},\\ \widehat{U}_x &= -\frac{2}{\mathcal{F}r} + \frac{6r}{m^2}\frac{\partial U}{\partial \bar{x}} + \frac{2r^2}{m^2}\frac{\partial^2 U}{\partial \bar{x} \partial r},\\ \widehat{U}_{rr} &= \frac{r^2}{m^2}\frac{\partial V}{\partial \bar{x}},\\ \widehat{U}_{xrr} &= \frac{2}{m^2}\left(\frac{1}{\mathcal{F}} - 2Vr - r^2\frac{\partial V}{\partial r}\right),\\ \widehat{U}_{xrr} &= \frac{2r}{m^2\mathcal{F}}. \end{split}$$

#### Appendix C. Modified block tridiagonal matrix algorithm 666

A modified block tridiagonal matrix algorithm is devised for solving the discretised version 667 of system (2.30)-(2.32) together with the discretised (2.20) for m = 0, 668

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671

$$A\delta = b. \tag{C1}$$

670 In expanded form, the system (C 1) is

 $\overline{C}$ 

$$\begin{bmatrix} A_{1} & C_{1} & & & & E_{1} \\ B_{2} & A_{2} & C_{2} & & & & E_{2} \\ & \cdots & \cdots & \cdots & & & \cdots & & \\ & & B_{j} & A_{j} & C_{j} & & & E_{j} \\ & & & \cdots & \cdots & & \cdots & & \cdots \\ & & & & B_{J-3} & A_{J-3} & C_{J-3} & E_{J-3} \\ D_{1} & D_{2} & D_{3} & & \cdots & & D_{J-2} & 0 \end{bmatrix} \begin{bmatrix} \delta_{1} \\ \delta_{2} \\ \vdots \\ \delta_{j} \\ \vdots \\ \delta_{J-3} \\ \delta_{J-2} \\ \Pi \end{bmatrix} = \begin{bmatrix} b_{1} \\ b_{2} \\ \vdots \\ b_{j} \\ \vdots \\ b_{J-3} \\ b_{J-2} \\ 0 \end{bmatrix}$$
(C 2)

where  $A_i$ ,  $B_i$  and  $C_i$  are  $3 \times 3$  matrices,  $E_i$ ,  $\delta_i$  and  $b_i$  are  $3 \times 1$  matrices,  $D_i$  is a  $1 \times 3$ 672 matrix, and  $\Pi$  is a scalar. In equation (C 2), row j for  $2 \le j \le J-3$  represents the discretised 673 equations (2.30)–(2.32) at the interior nodes, while rows 1 and J - 2 refer to the equations at 674 the boundaries. The last row is the discretised integral (2.20). 675

First, we add any two decoupled equations to the system in order to add two rows at the 676 bottom of matrix A and two columns on the right of matrix A. This step makes  $D_i$  and  $E_i$ 677 678  $3 \times 3$  matrices, and creates two  $3 \times 1$  matrices,  $\delta_{J-1}$  and  $b_{J-1}$ , at the bottom of  $\delta$  and **b**, which

is necessary in order to render the system suitable for the block elimination. The matrices 679

680  $D_j$  and  $E_j$  are renamed  $\mathcal{D}_j$  and  $\mathcal{E}_j$ . The system (C 2) becomes

681

The standard block tridiagonal matrix algorithm described in Cebeci (2002) is modified to solve (C 3), which also consists of the forward sweep and backward substitution. However, in each forward sweep, one more step needs to be performed to eliminate  $\mathcal{D}_i$ , which leads to

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688

where the prime denotes the new coefficients. The solution is then obtained by backwardsubstitution:

 $\begin{cases} \delta_{J-1} = \mathcal{E}_{J-1}^{\prime - 1} b_{J-1}^{\prime}, \\ \delta_{J-2} = b_{J-2}^{\prime} - \mathcal{E}_{J-2}^{\prime} \delta_{J-1}, \\ \delta_{i} = b_{i}^{\prime} - C_{i}^{\prime} \delta_{i+1} - \mathcal{E}_{i}^{\prime} \delta_{J-1}, \quad i = J - 3, J - 4, \cdots, 1. \end{cases}$ (C5)

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